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### **separation bubble Experiments on a two**−**dimensional laminar**

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C. P. Häggmark, A. A. Bakchinov and P. H. Alfredsson

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# $\frac{1.2000.0704}{\text{Experiments on a two-dimensional}$  laminar separation bubbleeriments on a two-dimensiona<br>laminar separation bubble

**laminar separation bubble**<br>By C. P. Häggmark†, A. A. Bakchinov‡ and P. H. Alfredsson *Department of Mechanics, KTH, S-100 44 Stockholm, Sweden*

 $E$  two-dimensional separation bubble on a flat plate is studied experimentally by<br>means of hot-wire anemometry and flow visualization. Separation of the laminar A two-dimensional separation bubble on a flat plate is studied experimentally by means of hot-wire anemometry and flow visualization. Separation of the laminar boundary layer on the plate is caused by an adverse pressure g A two-dimensional separation bubble on a flat plate is studied experimentally by means of hot-wire anemometry and flow visualization. Separation of the laminar boundary layer on the plate is caused by an adverse pressure g means of hot-wire anemometry and flow visualization. Separation of the laminar<br>boundary layer on the plate is caused by an adverse pressure gradient imposed by<br>a curved wall opposite to the plate. The instability of, and t a curved wall opposite to the plate. The instability of, and transition process in, a curved wall opposite to the plate. The instability of, and transition process in,<br>the separation bubble are focused on. The bubble is found to be highly susceptible<br>to high-frequency two-dimensional instability waves, wh the separation bubble are focused on. The bubble is found to be highly susceptible<br>to high-frequency two-dimensional instability waves, which are studied under both<br>natural and forced conditions. A similar development of t to high-frequency two-dimensional instability waves, which are studied under both natural and forced conditions. A similar development of these instability waves in the separation bubble is found in both cases. The exponen natural and forced conditions. A similar development of these instability waves in the separation bubble is found in both cases. The exponential growth of the two-<br>dimensional disturbances dominates the flow except for in the separation bubble is found in both cases. The exponential growth of the two-<br>dimensional disturbances dominates the flow except for in the reattachment region,<br>where large-scale three-dimensional structures appear. Som dimensional disturbances dominates the flow except for in the reattachment region, where large-scale three-dimensional structures appear. Some difficulties associated with experimental investigations of boundary-layer sepa cussed. with experimental investigations of boundary-layer separation-bubble flows are discussed.<br>Keywords: laminar separation bubbles; instability waves;

laminar turbulent transition; reattachment

#### 1. Introduction

This paper is concerned with the separation of a laminar boundary layer due to an This paper is concerned with the separation of a laminar boundary layer due to an<br>adverse pressure gradient and the transition from laminar to turbulent flow. The<br>laminar (transitional) separation bubble has previously bee This paper is concerned with the separation of a laminar boundary layer due to an adverse pressure gradient and the transition from laminar to turbulent flow. The laminar (transitional) separation bubble has previously bee adverse pressure gradient and the transition from laminar to turbulent flow. The laminar (transitional) separation bubble has previously been studied with different approaches—theoretical, numerical and experimental—which laminar (transitional) separation bubble has previously been studied with different<br>approaches—theoretical, numerical and experimental—which have given insight into<br>this complex flow field, but a description of the transit approaches—theoretical, numerical and experimental—which have given insight into<br>this complex flow field, but a description of the transition process in the separation<br>bubble is far from complete. In fact, experimental stu this complex flow field, but a description of the transition process in the separation<br>bubble is far from complete. In fact, experimental studies focusing on the transition<br>process in adverse-pressure-gradient-induced lami bubble is far from complete. In fact, experimental studies focusing on the transition process in adverse-pressure-gradient-induced laminar separation bubbles are scarce, despite the importance of this flow in many engineer process in adverse-pressure-gradient-induced laminar separation bubbles are scarce, despite the importance of this flow in many engineering applications. This can probably be explained partly by the difficulties with, and despite the importance of this flow in many engineering applications. This can prob-It is explained partly by the difficulties with, and shortcomings of, the available<br>easurement techniques for separated flows in general.<br>A schematic picture of the flow studied is given in figure 1, in which the wall-<br>rma

measurement techniques for separated flows in general.<br>A schematic picture of the flow studied is given in figure 1, in which the wall-<br>normal direction has been stretched for clarity. A low-velocity region, termed the<br>sep A schematic picture of the flow studied is given in figure 1, in which the wall-<br>normal direction has been stretched for clarity. A low-velocity region, termed the<br>separation bubble, is surrounded by a separated shear laye normal direction has been stretched for clarity. A low-velocity region, termed the separation bubble, is surrounded by a separated shear layer, which reattaches to the surface downstream of the bubble. Separation of the la separation bubble, is surrounded by a separated shear layer, which reattaches to<br>the surface downstream of the bubble. Separation of the laminar boundary layer is<br>caused by a retardation of the external flow due to an adve the surface downstream of the bubble. Separation of the laminar boundary layer is<br>caused by a retardation of the external flow due to an adverse pressure gradient.<br>The point of separation and the forward portion of the bub caused by a retardation of the external flow due to an adverse pressure gradient.<br>The point of separation and the forward portion of the bubble are steady compared with the highly unsteady flow in the vicinity of the reatt pared with the highly unsteady flow in the vicinity of the reattachment point. The † Present address: Volvo Car Cooperation, S-40531 Göteborg, Sweden.

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teborg Sweden † Present address<br>‡ Present address<br>Göteborg, Sweden. *G*öteborg, Sweden.<br>*Phil. Trans. R. Soc. Lond.* A (2000) **358**, 3193–3205

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Figure 1. Laminar separation-bubble flow due to an adverse pressure gradient.

separation bubble depicted in figure 1 should be distinguished from the case where<br>boundary-layer separation is caused by sharp gradients of the wall surface: geometryseparation bubble depicted in figure 1 should be distinguished from the case where<br>boundary-layer separation is caused by sharp gradients of the wall surface: geometry-<br>induced separation. The differences in the physics of boundary-layer separation is caused by sharp gradients of the wall surface: geometry-<br>induced separation. The differences in the physics of the flow between these two boundary-layer separation is caused by sharp gradients of the wall surface: geometry-<br>induced separation. The differences in the physics of the flow between these two<br>cases of separation are discussed by Alving & Fernholz ses of separation are discussed by Alving & Fernholz (1996) and Dovgal *et al.*<br>
In early experimental work on laminar separation bubbles, much effort was devoted<br>
determining empirical correlations between global quantit

(1994).<br>In early experimental work on laminar separation bubbles, much effort was devoted<br>to determining empirical correlations between global quantities of the bubble and<br>houndary-layer properties at the point of separat In early experimental work on laminar separation bubbles, much effort was devoted<br>to determining empirical correlations between global quantities of the bubble and<br>boundary-layer properties at the point of separation, and boundary-layer properties at the point of separation, and devising semi-empirical theories for predicting what kind of bubble would occur in a given flow situation. A review is given by Tani (1964). The effect of laminar separation bubbles on the stalling characteristics of different aerofoils was also tion. A review is given by Tani  $(1964)$ . The effect of laminar separation bubbles 1963).

Gaster (1966) investigated laminar separation bubbles on a flat plate caused by 1963).<br>Gaster (1966) investigated laminar separation bubbles on a flat plate caused by<br>an adverse pressure gradient for a broad range of Reynolds numbers and pressure<br>distributions. The pressure gradient was established by Gaster (1966) investigated laminar separation bubbles on a flat plate caused by<br>an adverse pressure gradient for a broad range of Reynolds numbers and pressure<br>distributions. The pressure gradient was established by an aer distributions. The pressure gradient was established by an aerofoil mounted above the flat plate. The aerofoil was equipped with a system for blowing through a slot at distributions. The pressure gradient was established by an aerofoil mounted above<br>the flat plate. The aerofoil was equipped with a system for blowing through a slot at<br>the surface in order to prevent stall. In contrast to the flat plate. The aerofoil was equipped with a system for blowing through a slot at<br>the surface in order to prevent stall. In contrast to the present investigation, where<br>a curved wall with suction was employed to produc the surface in order to prevent stall. In contrast to the present investigation, where<br>a curved wall with suction was employed to produce the adverse pressure gradi-<br>ent, this arrangement causes disturbances in the externa a curved wall with suction was employed to produce the adverse pressure gradient, this arrangement causes disturbances in the external stream, originating from the jet and the trailing-edge wake of the aerofoil, which can ent, this arrangement causes disturbances in the external stream, originating from<br>the jet and the trailing-edge wake of the aerofoil, which can influence the separated<br>region at the plate. Gaster (1966) found that the len the jet and the trailing-edge wake of the aerofoil, which can influence the separated<br>region at the plate. Gaster (1966) found that the length of the separation bubble<br>suddenly increased when the adverse pressure gradient region at the plate. Gaster (1966) found that the length of the separation bubble suddenly increased when the adverse pressure gradient and/or the Reynolds number exceeded certain critical values: so-called bubble bursting suddenly increased when the adverse pressure gradient and/or the Reynolds num-<br>ber exceeded certain critical values: so-called bubble bursting. Pauley *et al.* (1990)<br>studied separation bubbles numerically by modelling Ga ber exceeded certain critical values: so-called bubble bursting. Pauley *et al.* (1990) studied separation bubbles numerically by modelling Gaster's experiment and found that the bursting was due to periodic vortex sheddi studied separation bubbles numerically by modelling Gaster's experiment and found<br>that the bursting was due to periodic vortex shedding from the bubble, and that the<br>longer bubble in Gaster's experiment was the result of that the bursting was due to periodic vortex shedding from the bubble, and that the longer bubble in Gaster's experiment was the result of time averaging of that shedding. Furthermore, Pauley *et al.* (1990) found that the longer bubble in Gaster's experiment was the result of time averaging of that shedding. Furthermore, Pauley *et al.* (1990) found that the shedding frequency agreed with the predicted most-amplified linear inviscid instab layer. th the predicted most-amplified linear inviscid instability of the separated shear<br>recent experiments and direct numerical simulations have shown that instabil-<br>r and unsteadiness of laminar separation bubbles arise from t

layer.<br>Recent experiments and direct numerical simulations have shown that instabil-<br>ity and unsteadiness of laminar separation bubbles arise from the growth of low-<br>amplitude instability waves in the boundary layer, a pro Recent experiments and direct numerical simulations have shown that instability and unsteadiness of laminar separation bubbles arise from the growth of low-<br>amplitude instability waves in the boundary layer, a process whi amplitude instability waves in the boundary layer, a process which can start upstream<br>of separation (Dovgal *et al.* 1994; Gruber *et al.* 1987; Rist & Maucher 1994; Hildings 1997).

## *A two-dimensional laminar separation bubble*<br>2. Some difficulties associated with experiments on<br>laminar separation bubbles ulties associated with experin<br>laminar separation bubbles

Iaminar separation bubbles<br>The experimentalist investigating laminar separation bubbles encounters several par-<br>ticular problems due to the complexity of separated flows. As a background we will The experimentalist investigating laminar separation bubbles encounters several par-<br>ticular problems due to the complexity of separated flows. As a background we will<br>briefly bring up some of these difficulties. The experimentalist investigating laminar seticular problems due to the complexity of s<br>briefly bring up some of these difficulties.<br>Hot-wire anemometry has been successf cular problems due to the complexity of separated flows. As a background we will<br>iefly bring up some of these difficulties.<br>Hot-wire anemometry has been successfully used to give accurate and detailed<br>easurements with high

briefly bring up some of these difficulties.<br>Hot-wire anemometry has been successfully used to give accurate and detailed<br>measurements with high time resolution and space resolution in transition exper-<br>iments featuring hi Hot-wire anemometry has been successfully used to give accurate and detailed measurements with high time resolution and space resolution in transition experiments featuring high-frequency disturbance waves with low amplitu measurements with high time resolution and space resolution in transition experiments featuring high-frequency disturbance waves with low amplitudes. However, conventional measurements using single hot-wire techniques in r iments featuring high-frequency disturbance waves with low amplitudes. However,<br>conventional measurements using single hot-wire techniques in reverse-flow regions<br>give erroneous results due to the insensitivity of the sens conventional measurements using single hot-wire techniques in reverse-flow regions give erroneous results due to the insensitivity of the sensor element to the direction of the flow. In regions with reverse flow, the veloc give erroneous results due to the insensitivity of the sensor element to the direction of the flow. In regions with reverse flow, the velocity signal will be folded, resulting,<br>for instance, in a mean velocity that is too high. Nevertheless, using hot-wire tech-<br>niques in laminar separation bubbles requires for instance, in a mean velocity that is too high. Nevertheless, using hot-wire techniques in laminar separation bubbles requires that the hot-wire probe be properly designed and of an appropriate size in order to avoid in niques in laminar separation bubbles requires that the hot-wire probe be properly designed and of an appropriate size in order to avoid interference with the bubble.<br>At the leading edge of a low-Reynolds number aerofoil, s designed and of an appropriate size in order to avoid interference with the bubble.<br>At the leading edge of a low-Reynolds number aerofoil, separation will take place<br>downstream of the suction peak where the boundary layer At the leading edge of a low-Reynolds number aerofoil, separation will take place<br>downstream of the suction peak where the boundary layer is very thin. A typical<br>size for a leading-edge bubble could be only a fraction of a downstream of the suction peak w<br>size for a leading-edge bubble could<br>a couple of millimetres in length.<br>A nother difficulty arises from the Another difficulty arises from the fact that the laminar separation bubble is highly<br>Another difficulty arises from the fact that the laminar separation bubble is highly<br>nsitive to various kinds of perturbations in the flo

a couple of millimetres in length.<br>Another difficulty arises from the fact that the laminar separation bubble is highly<br>sensitive to various kinds of perturbations in the flow: both disturbances in the exter-<br>nal stream, s Another difficulty arises from the fact that the laminar separation bubble is highly sensitive to various kinds of perturbations in the flow: both disturbances in the external stream, such as mean flow variations, acousti sensitive to various kinds of perturbations in the flow: both disturbances in the external stream, such as mean flow variations, acoustic disturbances, freestream turbu-<br>lence, etc.; and surface vibrations and roughness. T nal stream, such as mean flow variations, acoustic disturbances, freestream turbu-<br>lence, etc.; and surface vibrations and roughness. This puts high demands on the<br>quality of the 'natural', i.e. unforced, flow in wind-tunn dence, etc.; and surface vibrations and roughness. This puts high demands on the quality of the 'natural', i.e. unforced, flow in wind-tunnel experiments in order to be able to isolate and quantitatively compare the effect quality of the 'natural', i.e. unforced, flow in wind-tunnel experiments in order to be able to isolate and quantitatively compare the effects of different types of artificially generated disturbances on the separated flow able to isolate and quantitatively compare the effects of different types of artificially

generated disturbances on the separated flow.<br>The laminar separation-bubble flow also shows an intrinsic unsteadiness. A small<br>variation in inflow conditions can result in unsteadiness and a considerable movement<br>of the se The laminar separation-bubble flow also shows an intrinsic unsteadiness. A small variation in inflow conditions can result in unsteadiness and a considerable movement of the separation point in the streamwise direction, bu variation in inflow conditions can result in unsteadiness and a considerable movement<br>of the separation point in the streamwise direction, but also in global changes of<br>the flow in the form of stochastic oscillations betwe of the separation point in the streamwise direction, but also in global changes of<br>the flow in the form of stochastic oscillations between separated and non-separated<br>flow. This can be caused by fluctuations in the adverse the flow in the form of stochastic oscillations between separated and non-separated<br>flow. This can be caused by fluctuations in the adverse pressure gradient, which<br>is usually applied by an auxiliary displacement body or s flow. This can be caused by fluctuations in the adverse pressure gradient, which<br>is usually applied by an auxiliary displacement body or suction slot. Even if the<br>separation point is steady, the two dimensionality is sensi is usually applied by an auxiliary displacement body or suction slot. Even if the separation point is steady, the two dimensionality is sensitive to pressure gradients in the spanwise direction, which will cause the separa separation point is steady, the two dimensionality is sensitive to pressure gradients

in the spanwise direction, which will cause the separation line to be curved.<br>In separated flows strong hysteresis effects can prevail, a complex phenomenon of which little is known. The structure of the separated flow the In separated flows strong hysteresis effects can prevail, a complex phenomenon of which little is known. The structure of the separated flow then depends on the flow history, for instance initial variations in pressure gra the start-up of the experiment. history, for instance initial variations in pressure gradient and Reynolds number at<br>the start-up of the experiment.<br>Together these factors make it complicated to establish experimental conditions<br>enabling accurate and rep

Together these factors make it complicated to establish experimental conditions.

#### 3. Experimental set-up and measurement technique

3. Experimental set-up and measurement technique<br>The measurements were carried out in the MTL wind tunnel at KTH, Stockholm.<br>This wind tunnel is designed for transition experiments, providing a low freestream The measurements were carried out in the MTL wind tunnel at KTH, Stockholm.<br>This wind tunnel is designed for transition experiments, providing a low freestream<br>turbulence level  $(Tu = 0.02\%)$  and acoustic noise level. In fi The measurements were carried out in the MTL wind tunnel at KTH, Stockholm.<br>This wind tunnel is designed for transition experiments, providing a low freestream<br>turbulence level  $(Tu = 0.02\%)$  and acoustic noise level. In fi

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rbulence level  $(Tu = 0.02\%)$  and acoustic noise level. In figure 2 a sketch of the<br>† The freestream turbulence level of the tunnel was determined with an empty test section at<br>m s<sup>-1</sup> for frequencies above 10 Hz, correspon  $25 \text{ m s}^{-1}$ , for frequencies above 10 Hz, corresponding to scales smaller than 2.5 m (see Johansson 1992). <sup>†</sup> The freestream turbulence level of the tunnel was determined with an empty test section at

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Figure 2. Experimental set-up in the MTL wind tunnel.

Figure 2. Experimental set-up in the MTL wind tunnel.<br>present test section set-up is shown. The height of the test section is 0.8 m and its<br>width is 1 2 m present test sectively width is 1.2 m. esent test section set-up is shown. The height of the test section is  $0.8$  m and its<br>dth is  $1.2$  m.<br>In the test section, a flat plate with an asymmetric leading edge and a trailing-<br> $\sigma$ e flan is installed. Further deta

width is 1.2 m.<br>In the test section, a flat plate with an asymmetric leading edge and a trailing-<br>edge flap is installed. Further details about the wind tunnel and the flat plate can be<br>found in Klingmann *et al.* (1993). In the test section, a flat plate with an asymmetric leading edge and a trailing-<br>edge flap is installed. Further details about the wind tunnel and the flat plate can be<br>found in Klingmann *et al.* (1993). An adverse press edge flap is installed. Further details about the wind tunnel and the flat plate can be<br>found in Klingmann *et al.* (1993). An adverse pressure gradient is imposed on the<br>laminar boundary layer on the plate by an adjustab found in Klingmann *et al.* (1993). An adverse pressure gradient is imposed on the laminar boundary layer on the plate by an adjustable contoured wall mounted in the test section. The contoured wall consisted of an alumin laminar boundary layer on the plate by an adjustable contoured wall mounted in the test section. The contoured wall consisted of an aluminium rig in which a 1 mm thick aluminium sheet was attached at one end and free to sl test section. The contoured wall consisted of an aluminium rig in which a 1 mm thick<br>aluminium sheet was attached at one end and free to slide at the other end. The<br>shape of the inserted wall could be changed by manually d aluminium sheet was attached at one end and free to slide at the other end. The shape of the inserted wall could be changed by manually displacing a threaded rod in the vertical direction. The end of this rod was connected shape of the inserted wall could be changed by manually displacing a threaded rod in<br>the vertical direction. The end of this rod was connected to an iron bar, horizontally<br>aligned and positioned perpendicular to the flow d the vertical direction. The end of this rod was connected to an iron bar, horizontally aligned and positioned perpendicular to the flow direction. This bar spanned the width of the test section and kept the aluminium sheet aligned and positioned perpendicular to the flow direction. This bar spanned the width of the test section and kept the aluminium sheet under tension and parallel to the flat plate.<br>In order to prevent separation at the cu width of the test section and kept the aluminium sheet under tension and parallel

to the flat plate.<br>In order to prevent separation at the curved wall, suction was applied through<br>a  $1.2 \times 0.3$  m<sup>2</sup> porous section of the aluminium sheet at the leeward side of the<br>contraction. The fraction of the flow i In order to prevent separation at the curved wall, suction was applied through a  $1.2 \times 0.3$  m<sup>2</sup> porous section of the aluminium sheet at the leeward side of the contraction. The fraction of the flow in the test section a  $1.2 \times 0.3$  m<sup>2</sup> porous section of the aluminium sheet at the leeward side of the contraction. The fraction of the flow in the test section removed through the porous section was *ca*. 0.5–1.0%. By applying suction, the contraction. The fraction of the flow in the test section removed through the porous section was  $ca. 0.5-1.0\%$ . By applying suction, the flow remained attached all along the curved wall. e curved wall.<br>The adverse pressure gradient, imposed by the contoured wall, causes the laminar<br>undary layer at the plate to separate. Reattachment of the unstable separated

the curved wall.<br>The adverse pressure gradient, imposed by the contoured wall, causes the laminar<br>boundary layer at the plate to separate. Reattachment of the unstable separated<br>shear layer further downstream results in th The adverse pressure gradient, imposed by the contoured wall, causes the laminar<br>boundary layer at the plate to separate. Reattachment of the unstable separated<br>shear layer further downstream results in the formation of a boundary layer at the plate to separate. Reattachment of the unstable separated shear layer further downstream results in the formation of a laminar separation shear layer further downstream results in the formation of a laminar separation<br>bubble with an average length and height of  $ca$ . 200 mm and  $ca$ . 3 mm, respectively.<br>This fairly large size of the separation bubble made det bubble with an average length and height of  $ca$ . 200 mm and  $ca$ . 3 mm, respectively.<br>This fairly large size of the separation bubble made detailed measurements in the bubble with a hot wire possible.<br>The streamwise veloci The streamwise velocity component of the flow in the separation bubble was mea-<br>The streamwise velocity component of the flow in the separation bubble was mea-<br>red with a 2.5 um platinum single hot wire which could be tra

sured with a  $2.5 \mu m$  platinum single hot wire, which could be traversed by a five-axis The streamwise velocity component of the flow in the separation bubble was measured with a  $2.5 \mu m$  platinum single hot wire, which could be traversed by a five-axis traversing system. Calibration was performed upstream o sured with a 2.5  $\mu$ m platinum single hot wire, which could be traversed by a five-axis traversing system. Calibration was performed upstream of the contraction against a Pitot tube connected to a highly accurate pressur traversing system. Calibration was performed upstream of the contraction against a<br>Pitot tube connected to a highly accurate pressure transducer. During calibration of<br>the probe and during measurements the ambient air tem Pitot tube connected to a highly accurate pressure transducer. During calibrat the probe and during measurements the ambient air temperature in the wind tunnel.<br>was kept constant within  $\pm 0.1$  °C by the cooling system o e probe and during measurements the ambient air temperature in the wind tunnel<br>is kept constant within  $\pm 0.1$  °C by the cooling system of the wind tunnel.<br>A Cartesian coordinate system is adopted with its origin on the

was kept constant within  $\pm 0.1$  °C by the cooling system of the wind tunnel.<br>A Cartesian coordinate system is adopted with its origin on the centreline at the leading edge of the plate. The velocity components in the st y, and spanwise, z, directions are denoted by  $u, v$  and  $w$ , respectively. and spanwise, z, directions are denoted by  $u$ ,  $v$  and  $w$ , respectively.<br>The boundary layer on the plate was traversed with the single hot wire, and<br>the single hot wire, and<br>the single hot wire, and<br>the single hot wire,

y, and spanwise, z, directions are denoted by  $u$ ,  $v$  and  $w$ , respectively.<br>The boundary layer on the plate was traversed with the single hot wire, and time traces of the anemometer signal were recorded at each measurem *Phil. Trans. R. Soc. Lond.* A (2000) *Phil. Trans. R. Soc. Lond.* A (2000)

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Figure 3. Streamwise variation of the edge velocity,  $U_e/U_{e0}$ .<br>
sampling frequency of 2.0 kHz. The streamwise spacing,  $\Delta x$ , between two consecutive<br>
profiles was 25–20 or 10 mm, with the denser spacing used in the latt sampling frequency of 2.0 kHz. The streamwise spacing,  $\Delta x$ , between two consecutive<br>profiles was 25, 20 or 10 mm, with the denser spacing used in the latter part of the<br>bubble  $\Delta x = 10$  mm corresponded to ca. 5% of the sampling frequency of 2.0 kHz. The streamwise spacing,  $\Delta x$ , between two consecutive<br>profiles was 25, 20 or 10 mm, with the denser spacing used in the latter part of the<br>bubble.  $\Delta x = 10$  mm corresponded to *ca*. 5% of t profiles was 25, 20 or 10 mm, with the denser spacing used in the latter part of the bubble.  $\Delta x = 10$  mm corresponded to *ca*. 5% of the total length of the separation bubble and a typical series of measurements consiste bubble and a typical series of measurements consisted of 30 vertical profiles, each containing  $20-40$  points depending on x.

blowing at the wall through a  $330 \times 0.8$  mm<sup>2</sup> slot in a flush-mounted plug in the plate. Controlled disturbances could be generated in the boundary layer by suction and The slot is located at  $x = 189$  mm, approximately three bubble lengths upstream blowing at the wall through a  $330 \times 0.8$  mm<sup>2</sup> slot in a flush-mounted plug in the plate.<br>The slot is located at  $x = 189$  mm, approximately three bubble lengths upstream<br>of the point of separation, perpendicularly aligne The slot is located at  $x = 189$  mm, approximately three bubble lengths upstream<br>of the point of separation, perpendicularly aligned to the direction of the flow. At<br>the lower side of the plug 40 inlet pipes are mounted, c of the point of separation, perpendicularly aligned to the direction of the flow. At<br>the lower side of the plug 40 inlet pipes are mounted, connected by flexible hoses to<br>loudspeakers. By feeding the loudspeakers with phas the lower side of the plug 40 inlet pipes are mounted, connected by flexible hoses to loudspeakers. By feeding the loudspeakers with phase- and amplitude-controlled signals generated by a computer, different types of wave loudspeakers. By feeding the loudspeakers with phase- and amplitude-controlled signals generated by a computer, different types of wave disturbances can be generated (see Elofsson 1998). The disturbance wave generation, th (see Elofsson 1998). The disturbance wave generation, the data acquisition and the

#### 4. Results

### $(a)$  *Mean flow*

The variation of the edge velocity,  $U_e$ , i.e. the velocity in the outer inviscid flow, along The variation of the edge velocity,  $U_e$ , i.e. the velocity in the outer inviscid flow, along<br>the plate is shown in figure 3.  $U_e$  is normalized with a reference velocity at the leading<br>edge  $U_e(x=0) = U_{e0} = 7 \text{ m s}^{-1}$  whi The variation of the edge velocity,  $U_e$ , i.e. the velocity in the outer inviscid flow, along<br>the plate is shown in figure 3.  $U_e$  is normalized with a reference velocity at the leading<br>edge,  $U_e(x = 0) = U_{e0} = 7$  m s<sup>-1</sup>, w the plate is shown in figure 3.  $U_e$  is normalized with a reference velocity at the leading edge,  $U_e(x = 0) = U_{e0} = 7 \text{ m s}^{-1}$ , which was kept constant in these experiments. The laminar boundary layer on the plate is first edge,  $U_e(x = 0) = U_{e0} = 7 \text{ m s}^{-1}$ , which was kept constant in these experiments. The laminar boundary layer on the plate is first accelerated, reaching a maximum velocity approximately at the throat of the contraction at laminar boundary layer on the plate is first accelerated, reaching a maximum velocity<br>approximately at the throat of the contraction at  $x \approx 550$  mm. Thereafter the flow is<br>decelerated, followed by separation. Outside the approximately at the throat of the contraction at  $x \approx 550$  mm. Thereafter the flow is<br>decelerated, followed by separation. Outside the separation bubble  $U_e$  becomes fairly<br>constant, a region referred to in the literatur decelerated, followed by separation. Outside the separation bubble  $U_e$  becomes fairly constant, a region referred to in the literature as the 'pressure plateau', since the static pressure at the wall becomes constant the constant, a region referred to in the literature as the 'pressure plateau', since the static pressure at the wall becomes constant there. Further downstream an abrupt decrease in  $U_e$  occurs, which is associated with reat static pressure at the wall becomes constant there. Further downstream an abrupt decrease in  $U_e$  occurs, which is associated with reattachment. Here, the separation point does not coincide with the beginning of the 'pres decrease in  $U_{\rm e}$  occu<br>point does not coin<br>further upstream. *Phil. Trans. R. Soc. Lond.* A (2000)



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velocity profiles along the plate centreline. Stream<br>are given in millimetres from the leading edge.

are given in millimetres from the leading edge.<br>Figure 4 shows profiles of the streamwise mean velocity component, normalized Figure 4 shows profiles of the streamwise mean velocity component, normalized with the edge velocity,  $U_e$ , at several downstream positions. The actual separation bubble appears as the part of the velocity profile pear th Figure 4 shows profiles of the streamwise mean velocity component, normalized with the edge velocity,  $U_e$ , at several downstream positions. The actual separation bubble appears as the part of the velocity profile near th with the edge velocity,  $U_e$ , at several downstream positions. The actual separation<br>bubble appears as the part of the velocity profile near the wall, where the velocity<br>seems to be independent of y and not approaching ze bubble appears as the part of the velocity profile near the wall, where the velocity seems to be independent of  $y$  and not approaching zero. This is due to the inability of the single wire to detect the flow direction. C seems to be independent of y and not approaching zero. This is due to the inability<br>of the single wire to detect the flow direction. Comparing, for example, the profiles at<br> $x = 860$  mm and at  $x = 900$  mm, the vertical ext % of the single wire to detect the flow<br> $x = 860$  mm and at  $x = 900$  mm,<br>is seen to increase downstream.<br>Due to the behaviour of the si-= 860 mm and at  $x = 900$  mm, the vertical extent of this constant velocity region<br>seen to increase downstream.<br>Due to the behaviour of the single wire in reverse-flow regions mentioned above,<br>e hot-wire measurements could

is seen to increase downstream.<br>Due to the behaviour of the single wire in reverse-flow regions mentioned above,<br>the hot-wire measurements could only give an approximate location of the separation<br>and reattachment points. Due to the behaviour of the single wire in reverse-flow regions mentioned above,<br>the hot-wire measurements could only give an approximate location of the separation<br>and reattachment points. These were more accurately dete the hot-wire measurements could only give an approximate location of the separation<br>and reattachment points. These were more accurately determined from smoke visu-<br>alizations. Separation and reattachment were hereby found and reattachment points. These were more accurately determined from smoke visu-<br>alizations. Separation and reattachment were hereby found to occur at  $x_s \approx 700$  mm<br>and  $x_r \approx 900$  mm, respectively. The Reynolds number base alizations. Separation and reattachment were hereby found to occur at  $x_s \approx 700$  mm<br>and  $x_r \approx 900$  mm, respectively. The Reynolds number based on  $U_{e0}$  and the distance<br>from the leading edge to the point of separation, d  $x_r \approx 900$  mm, respectively. The Reynolds number based on  $U_{e0}$  and the distance<br>om the leading edge to the point of separation,  $x_s$ , was  $Re_x = U_{e0}x_s/\nu = 3.3 \times 10^5$ .<br>The variation with x of the integral flow paramete

ness  $\delta^*$ , is leading edge to the point of separation,  $x_s$ , was  $Re_x = U_{e0}x_s/\nu = 3.3 \times 10^5$ .<br>variation with x of the integral flow parameters—i.e. the displacement thick-<br>the momentum loss thickness  $\theta$  and shape factor,  $H = \delta^*/\theta$ The variation with x of the integral flow parameters—i.e. the displacement thickness  $\delta^*$ , the momentum loss thickness  $\theta$  and shape factor,  $H = \delta^*/\theta$ —is illustrated in figure 5. The Reynolds numbers based on the edge ¤ ness  $\theta$  and shape factor,  $H = \delta^*/\theta$ —is illustrated<br>rrs based on the edge velocity at separation,  $U_s$ ,<br> $\frac{k}{s}$  or momentum thickness at separation,  $\theta_s$ , were

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Figure 5. Integral flow parameters:  $-\circ-\circ$ ,  $\delta^*$  (mm);  $-*$ ,  $\theta$  (mm);  $\_\_\_\$ ,  $H$ .<br>  $Re_{\delta^*_{\epsilon}} = 1390$  and  $Re_{\theta_s} = 417$ , respectively. Inside the region of the bubble,  $\theta$  remains<br>
fairly constant in comparison with  $Re_{\delta_{\rm s}^*} = 1390$  and  $Re_{\theta_{\rm s}} = 417$ , respectively. Inside the region of the bubble,  $\theta$  remains fairly constant in comparison with  $\delta^*$ . Not until  $x \approx 870$  mm does  $\theta$  increase as the unstable separated shear l airly constant in comparison with  $\delta^*$ . Not until  $x \approx 870$  mm does  $\theta$  increase as the nstable separated shear layer reattaches and a turbulent boundary layer develops.<br>\* on the other hand shows an enhanced growth ups  $Re_{\delta_s^*} = 1390$  and  $Re_{\theta_s} = 417$ , respectively. Inside the region of the bubble,  $\theta$  remains fairly constant in comparison with  $\delta^*$ . Not until  $x \approx 870$  mm does  $\theta$  increase as the unstable separated shear layer re  $\delta^*$  on the other hand shows an enhanced growth upstream of the separation point, unstable separated shear layer reattaches and a turbulent boundary layer develops.<br> $\delta^*$  on the other hand shows an enhanced growth upstream of the separation point,<br>reaching a maximum value at  $x = 860$  mm, and from ther  $\delta^*$  on the other hand shows an enhanced growth upstream of the separation point, reaching a maximum value at  $x = 860$  mm, and from there on decays as the mean velocity profile gets fuller. The shape factor reaches a ma reaching a maximum value at  $x = 860$  mm, and from there on decays as the mean<br>velocity profile gets fuller. The shape factor reaches a maximum value of approxi-<br>mately 5 in the separation bubble. Since no backflow is meas velocity profile gets fuller. The shape factor reaches a maximum value of approximately 5 in the separation bubble. Since no backflow is measured in the reverse-flow region in the bubble,  $\delta^*$  will be underestimated and where The shape factor reaches a maximum value of approxition bubble. Since no backflow is measured in the reverse-flow  $*$  will be underestimated and  $\theta$  overestimated in the numerical an velocity profiles in the bubble mately 5 in the separation bubble. Since no backflow is measured in the reverse-flow<br>region in the bubble,  $\delta^*$  will be underestimated and  $\theta$  overestimated in the numerical<br>integrations of the mean velocity profiles i region in the bubble,  $\delta^*$  will be underestimated and  $\theta$  overestimated in the numerical integrations of the mean velocity profiles in the bubble. The values in figure 5 should therefore be considered as indicative, an therefore be considered as indicative, and should not be used for determining the points of separation and reattachment.

#### (*b*) *Natural velocity fluctuations*

The natural, i.e. unforced, laminar separation-bubble flow in the present investi-The natural, i.e. unforced, laminar separation-bubble flow in the present investigation is highly unstable. Initially disturbances in the boundary layer are damped in the favourable-pressure-gradient region unstream of th The natural, i.e. unforced, laminar separation-bubble flow in the present investigation is highly unstable. Initially disturbances in the boundary layer are damped in the favourable-pressure-gradient region upstream of the gation is highly unstable. Initially disturbances in the boundary layer are damped in<br>the favourable-pressure-gradient region upstream of the bubble, but further down-<br>stream the rapid disturbance growth in the adverse-pre the favourable-pressure-gradient region upstream of the bubble, but further down-<br>stream the rapid disturbance growth in the adverse-pressure-gradient boundary layer<br>and in the separated shear layer causes transition and a stream the rapid disturbance ground in the separated shear layer<br>established after reattachment.<br>Figure 6 shows amplitude specand in the separated shear layer causes transition and a turbulent boundary layer is established after reattachment.<br>Figure 6 shows amplitude spectra of the streamwise velocity inside the separated

established after reattachment.<br>Figure 6 shows amplitude spectra of the streamwise velocity inside the separated<br>shear layer at  $x = 830, 840$  and 850 mm. The dominating natural velocity fluctuations<br>in the separated shear Figure 6 shows amplitude spectra of the streamwise velocity inside the separated shear layer at  $x = 830$ , 840 and 850 mm. The dominating natural velocity fluctuations in the separated shear layer in the bubble have dispar shear layer at  $x = 830$ , 840 and 850 mm. The dominating natural velocity fluctuations<br>in the separated shear layer in the bubble have disparate time-scales. The natural<br>fluctuations can broadly be divided into low-frequen in the separated shear layer in the bubble have disparate time-scales. The natural fluctuations can broadly be divided into low-frequency oscillations (here frequencies less than 20 Hz) and high-frequency oscillations (in fluctuations can broadly be divided into low-frequency oscillations (here frequencies<br>less than 20 Hz) and high-frequency oscillations (in this case frequencies in the range<br>60–120 Hz). The presence of low-frequency fluctu less than 20 Hz) and high-frequency oscillations (in this case frequencies in the range  $60-120$  Hz). The presence of low-frequency fluctuations in the separation bubble is a characteristic feature of separated flows in g 60–120 Hz). The presence of low-frequency fluctuations in the separation bubble is a characteristic feature of separated flows in general, and is not restricted to the case where separation is caused by an adverse pressure where separation is caused by an adverse pressure gradient (Cherry *et al.* 1984). The

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Figure 6. Amplitude spectra of streamwise velocity,  $A_u(f)$ , in the separated shear layer at  $x = 830$ , 840 and 850 mm and  $y = 5.2$  mm under natural conditions. The spectra are shifted in Figure 6. Amplitude spectra of streamwise vel  $x = 830$ , 840 and 850 mm and  $y = 5.2$  mm under amplitude by a factor of  $0.5 \times 10^{-3}$  for clarity.

amplitude by a factor of  $0.5 \times 10^{-8}$  for clarity.<br>instability, which is especially manifested in the reattachment region and gives rise<br>to an overall 'flapping' motion of the separated shear layer, observed by Dovgal *e* instability, which is especially manifested in the reattachment region and gives rise<br>to an overall 'flapping' motion of the separated shear layer, observed by Dovgal  $et$ <br> $al$  (1994) among others. The high-frequency fluctu instability, which is especially manifested in the reattachment region and gives rise<br>to an overall 'flapping' motion of the separated shear layer, observed by Dovgal *et*<br>*al.* (1994) among others. The high-frequency fluc to an overall 'flapping' motion of the separated shear layer, observed by Dovgal *et al.* (1994) among others. The high-frequency fluctuations in figure 6 are seen to increase downstream, which illustrates that naturally this frequency range grow rapidly.

### (*c*) *Artificially forced instability waves*

 $(c)$  *Artificially forced instability waves*<br>The development of low-amplitude two-dimensional instability waves in the sepa-<br>tion bubble was investigated further by means of controlled generation by suction The development of low-amplitude two-dimensional instability waves in the separation bubble was investigated further by means of controlled generation by suction and blowing through the transverse slot in the plate locate The development of low-amplitude two-dimensional instability waves in the separation bubble was investigated further by means of controlled generation by suction and blowing through the transverse slot in the plate locate ration bubble was investigated further by means of controlled generation by suction<br>and blowing through the transverse slot in the plate located at  $x = 189$  mm. When<br>using artificial excitation a phase reference exists, a and blowing through the transverse slot in the plate located at  $x = 189$  mm. When<br>using artificial excitation a phase reference exists, and the downstream development<br>of the phase of the instability wave was chosen to agr using artificial excitation a phase reference exists, and the downstream development<br>of the phase of the instability wave can be measured with one probe. The frequency<br>of the forced instability wave was chosen to agree wi % of the phase of the instability wave can be measur<br>of the forced instability wave was chosen to agre<br>frequencies in the natural bubble,  $f^* = 83.3 \text{ Hz}$ .<br>Close to the disturbance source the instability w the forced instability wave was chosen to agree with one of the most amplified equencies in the natural bubble,  $f^* = 83.3 \text{ Hz}$ .<br>Close to the disturbance source the instability wave resembles a Tollmien-Schlich-<br>or wave

frequencies in the natural bubble,  $f^* = 83.3 \text{ Hz}$ .<br>Close to the disturbance source the instability wave resembles a Tollmien–Schlich-<br>ting wave in the Blasius boundary layer with two local maxima in the amplitude dis-<br>t Close to the disturbance source the instability wave resembles a Tollmien–Schlich-<br>ting wave in the Blasius boundary layer with two local maxima in the amplitude dis-<br>tribution of the fluctuating streamwise velocity. When ting wave in the Blasius boundary layer with two local maxima in the amplitude dis-<br>tribution of the fluctuating streamwise velocity. When entering the separated region,<br>the amplitude distribution of the instability wave c tribution of the fluctuating streamwise velocity. When entering the separated region, the amplitude distribution of the instability wave changes shape and develops a third local maximum in the shear layer. Similar behaviou the amplitude distribution of the instability wave changes shape and develops a<br>third local maximum in the shear layer. Similar behaviour was observed for the nat-<br>urally excited high-frequency waves prior to reattachment. third local maximum in the shear layer. Similar behaviour was observed for the naturally excited high-frequency waves prior to reattachment. Figure 7 compares the wall-normal distribution of the amplitude of the forced wav urally excited high-frequency waves prior to reattachment. Figure 7 compares the wall-normal distribution of the amplitude of the forced wave at three streamwise positions close to reattachment with a filtered RMS distribu wall-normal distribution of the amplitude of the forced wave at three streamwise<br>positions close to reattachment with a filtered RMS distribution of the fluctuating<br>streamwise velocity in the natural case, where the time positions close to reattachment with a filtered RMS distribution of the fluctuating<br>streamwise velocity in the natural case, where the time signals were bandpass filtered<br>in the range 40–133 Hz. The corresponding mean velo in the range 40–133 Hz. The corresponding mean velocity profiles are plotted in the same graphs. The three maxima are, both in the natural case and in the forced case,

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Figure 7. Amplitude profiles of natural and forced instability waves prior to reattachment.<br>Measurements at  $x = 880$  ( $\text{-} \text{o} - \text{o} -$ ), 890 ( $\text{=} \text{**}$ ) and 900 mm ( $\text{=} \nabla \text{=} \nabla$ ) in the natural flow case (a) Figure 7. Amplitude profiles of natural and forced instability waves prior to reatta<br>Measurements at  $x = 880$  (-o-o-), 890 (-\*-\*-) and 900 mm (- $\triangledown - \triangledown -$ ) in the natural fl<br>(a), and at  $x = 830$  (-o-o-), 840 (-\*-\*-) and

(a), and at  $x = 830$  (-o-o-), 840 (-\*-\*-) and 850 mm (- $\nabla$ - $\nabla$ -) in the forced case (b).<br>located at the edge of the low-velocity region, at the inflection point of the separated<br>shear layer, and at its edge, respectiv located at the edge of the low-velocity regionshear layer, and at its edge, respectively.<br>Figure 8 shows the wall-normal phase cated at the edge of the low-velocity region, at the inflection point of the separated<br>ear layer, and at its edge, respectively.<br>Figure 8 shows the wall-normal phase profile of the forced instability wave at<br> $= 840$  mm (b

shear layer, and at its edge, respectively.<br>Figure 8 shows the wall-normal phase profile of the forced instability wave at  $x = 840$  mm (b) together with the streamwise phase variation of the middle amplitude maximum of the wave (a). Two phase shifts exist in the phase profile at  $x = 840$  mm,  $x = 840$  mm (b) together with the streamwise phase variation of the middle amplitude maximum of the wave (a). Two phase shifts exist in the phase profile at  $x = 840$  mm, located between regions of constant phase, which co maximum of the wave  $(a)$ . Two phase shifts exist in the phase profile at  $x = 840$  mm, located between regions of constant phase, which correspond to the three local amplitude maxima seen in figure 7. From the downstream p *Phil. Trans. R. Soc. Lond.* A (2000)

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Figure 8. Phase development (the phase is determined at the middle maxima) in the streamwise direction (*a*) and wall-normal phase profile at  $x = 840$  mm (*b*) of the two-dimensional instability wave in the separation bub direction (a) and wall-normal phase profile at  $x = 840$  mm (b) of the two-dimensional instability wave in the separation bubble. The frequency is 83.3 Hz.

amplitude maximum, the phase speed, <sup>c</sup>, of the instability waves can be determined as

$$
c = \omega / \frac{\Delta \phi}{\Delta x},
$$

 $c = \omega / \frac{\overline{\Delta x}}{\Delta x}$ ,<br>where  $\omega = 2\pi f^*$ , c is found to be nearly constant in the region where the separation<br>bubble is located until reattachment occurs. At  $x = 840$  mm,  $c/U_s = 0.39$ . This is where  $\omega = 2\pi f^*$ . c is found to be nearly constant in the region where the separation<br>bubble is located until reattachment occurs. At  $x = 840$  mm,  $c/U_e = 0.39$ . This is<br>lower than the mean velocity at the inflection poin where  $\omega = 2\pi f^*$ . c is found to be nearly constant in the region where the separation<br>bubble is located until reattachment occurs. At  $x = 840$  mm,  $c/U_e = 0.39$ . This is<br>lower than the mean velocity at the inflection poin bubble is located until reattachment occurs. At  $x = 840$  mm,  $c/U_e = 0.39$ . This is lower than the mean velocity at the inflection point at the same streamwise position, which equals  $0.60U_e$ . One may have expected that the lower than the mean velocity at the inflection point at the same streamwise position,<br>which equals  $0.60U_e$ . One may have expected that the phase speed of the waves<br>would be closer to the mean velocity at the inflection p which equals  $0.60U_e$ . One may have expected that the phase speed of the waves<br>would be closer to the mean velocity at the inflection point as would be the case in<br>a free shear layer flow, but, as Michalke (1990) has show would be closer to the mean velocity at the inflection point as would be the case in<br>a free shear layer flow, but, as Michalke (1990) has shown, the influence of the wall<br>reduces the wave speed quite significantly for wave a free shear layer flow, but, as Michalke (1990) has shown, the influence of the wall<br>reduces the wave speed quite significantly for wavelengths that are larger than the<br>distance of the inflection point from the wall. In f reduces the wave speed quite significantly for wavelengths that are larger than the distance of the inflection point from the wall. In fact, our measured phase speed is close to values corresponding to his numerical result distance of the inflection point from the wall. In fact, our measured phase speed is

close to values corresponding to his numerical results.<br>The streamwise growth of the forced two-dimensional wave is shown in figure 9.<br>The instability wave grows exponentially between  $x \approx 700$  and  $x \approx 825$  mm and sat-<br>u The streamwise growth of the forced two-dimensional wave is shown in figure 9.<br>The instability wave grows exponentially between  $x \approx 700$  and  $x \approx 825$  mm and saturates after reattachment at an amplitude above 10%. This g urates after reattachment at an amplitude above 10%. This growth starts upstream<br>of separation, in the adverse pressure gradient boundary layer, where a factor 5<br>increase in amplitude is observed from  $x \approx 600$  to  $x_s \approx 7$ urates after reattachment at an amplitude above 10%. This growt<br>of separation, in the adverse pressure gradient boundary layer,<br>increase in amplitude is observed from  $x \approx 600$  to  $x_s \approx 700$  mm.<br>The disturbance growth in separation, in the adverse pressure gradient boundary layer, where a factor 5<br>crease in amplitude is observed from  $x \approx 600$  to  $x_s \approx 700$  mm.<br>The disturbance growth in the bubble is quite high; the separation bubble has<br>

increase in amplitude is observed from  $x \approx 600$  to  $x_s \approx 700$  mm.<br>The disturbance growth in the bubble is quite high; the separation bubble has<br>the ability to amplify the wave by almost three orders of magnitude in a str The disturbance growth in the bubble is quite high; the separation<br>the ability to amplify the wave by almost three orders of magnitude in a<br>distance of 200 mm, corresponding to approximately five wavelengths. distance of 200 mm, corresponding to approximately five wavelengths.<br>(*d*) *Flow visualizations* 

The flow in the separation bubble was visualized by introducing a thin layer of smoke through a narrow slot in the plate 212 mm downstream of the leading edge. The flow in the separation bubble was visualized by introducing a thin layer of smoke through a narrow slot in the plate 212 mm downstream of the leading edge.<br>A photograph of the flow in the case of natural transition is smoke through a narrow slot in the plate  $212 \text{ mm}$  downstream of the leading edge.<br>A photograph of the flow in the case of natural transition is shown in figure 10.<br>The flow is from left to right and the scale in the upp A photograph of the flow in the case of natural transition is shown in figure 10.<br>The flow is from left to right and the scale in the upper part of the photograph is<br>in mm, with zero at the leading edge. In the laminar bou The flow is from left to right and the scale in the upper part of the photograph is<br>in mm, with zero at the leading edge. In the laminar boundary layer ahead of the<br>bubble, the smoke sheet is smooth and unperturbed. The s in mm, with zero at the leading edge. In the laminar boundary layer ahead of the bubble, the smoke sheet is smooth and unperturbed. The separation line can be seen around  $x = 700$  mm. The bubble remains fairly two dimensi bubble, the smoke sheet is smooth and unperturbed. The separation line can be seen<br>around  $x = 700$  mm. The bubble remains fairly two dimensional and steady from<br>the point of separation up to  $x \approx 860$  mm. Before the reatt

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ication curve of forced two-dimensional inst<br>the separation bubble with  $f^* = 83.3$  Hz.



Figure 10. Instantaneous smoke visualization of the separation bubble under natural conditions.

crests can be distinguished, whereafter the smoke sheet is dispersed, although a weak<br>three-dimensional structure is visible three-dimensional structure is visible.<br>In figure 11 the flow is forced through three-dimensional structure is visible.<br>In figure 11 the flow is forced through the slot at  $x = 189$  mm with a frequency

three-dimensional structure is visible.<br>In figure 11 the flow is forced through the slot at  $x = 189$  mm with a frequency<br>of 102 Hz. For this case several waves can be seen, which are initially highly two<br>dimensional. The In figure 11 the flow is forced through the slot at  $x = 189$  mm with a frequency<br>of 102 Hz. For this case several waves can be seen, which are initially highly two<br>dimensional. The breakup occurs at almost constant x acro of 102 Hz. For this case several waves can be seen, which are initially highly two<br>dimensional. The breakup occurs at almost constant  $x$  across the full span of the<br>smoke sheet, and here a three-dimensional streamwise or dimensional. The breakup occurs at almost constant  $x$  across the full span of the smoke sheet, and here a three-dimensional streamwise oriented pattern is clearly seen in and after the reattachment region. From video rec seen in and after the reattachment region. From video recordings it was observed that the three-dimensional structure was fairly steady in the spanwise direction and had a spanwise wavelength of  $ca$ . 30 mm. that the three-dimensional structure was fairly steady in the spanwise direction and

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Figure 11. Instantaneous smoke visualization of the separation bubble when forcing a Figure 11. Instantaneous smoke visualization of the separation bubble when forcing a two-dimensional instability wave.  $U_{e0} = 5.0 \text{ m s}^{-1}$  and the forcing frequency is 102 Hz. the sum of the separation  $5.$  Summary and conclusions

5. Summary and conclusions<br>A two-dimensional laminar separation bubble induced by an adverse-pressure gradi-A two-dimensional laminar separation bubble induced by an adverse-pressure gradient was studied experimentally in a wind tunnel. The set-up employed a contoured wall with boundary-layer suction to induce the pressure gradi A two-dimensional laminar separation bubble induced by an adverse-pressure gradient was studied experimentally in a wind tunnel. The set-up employed a contoured wall with boundary-layer suction to induce the pressure gradi ent was studied experimentally in a wind tunnel. The set-up employed a contoured wall with boundary-layer suction to induce the pressure gradient and resulted in<br>a bubble with a stable, two-dimensional separation line. The wall with boundary-layer suction to induce the pressure gradient and resulted in<br>a bubble with a stable, two-dimensional separation line. The present experiments<br>combine flow visualization, hot-wire measurements and an acc forcing technique to make detailed measurements of the evolution of single-frequency combine flow visualization, hot-wire measurements and an accurate wave disturbance<br>forcing technique to make detailed measurements of the evolution of single-frequency<br>two-dimensional instability waves in the separating an forcing technique to make detailed measurements of<br>two-dimensional instability waves in the separating<br>as well as naturally occurring wave disturbances.<br>The present investigation is in qualitative agreement o-dimensional instability waves in the separating and reattaching boundary layer,<br>well as naturally occurring wave disturbances.<br>The present investigation is in qualitative agreement with previous studies on lami-<br>r separa

as well as naturally occurring wave disturbances.<br>The present investigation is in qualitative agreement with previous studies on lami-<br>nar separation, but is unique in its set-up and level of detailed measurements. Several The present investigation is in qualitative agreement with previous studies on laminar separation, but is unique in its set-up and level of detailed measurements. Several new interesting aspects of disturbance growth were mar separation, but is<br>new interesting aspec<br>main results below. new interesting aspects of disturbance growth were also observed. We summarize the main results below.<br>(1) The streamwise velocity disturbance distribution for both natural and forced

- The streamwise velocity disturbance distribution for both natural and forced<br>disturbances shows three maxima. The largest amplitude corresponds to the<br>inflection point in the mean velocity, indicating an inviscid origin of The streamwise velocity disturbance distribution for both natural and forced disturbances shows three maxima. The largest amplitude corresponds to the inflection point in the mean velocity, indicating an inviscid origin of turbance.
- (2) The phase speed of the disturbance is lower than the velocity at the inflection<br>noint. This is probably an effect of the wall, which has theoretically been shown The phase speed of the disturbance is lower than the velocity at the inflection<br>point. This is probably an effect of the wall, which has theoretically been shown<br>to lower the phase speed as compared with a free shear layer The phase speed of the disturbance is lower than the velocity at the inflection point. This is probably an effect of the wall, which has theoretically been shown to lower the phase speed as compared with a free shear layer
- (3) The growth rate of wave disturbances in the bubble was found to be exponen-<br>tial and the wave amplitude of the forced wave reaches a value of  $ca$  10% of the growth rate of wave disturbances in the bubble was found to be exponential, and the wave amplitude of the forced wave reaches a value of *ca*. 10% of the edge velocity before it saturates. These results are in excellen The growth rate of wave disturbances in the bubble was found to be exponential, and the wave amplitude of the forced wave reaches a value of  $ca.10\%$  of the edge velocity before it saturates. These results are in excellen tial, and the wave amplitude of the forced wave reaches a value of  $ca.10\%$  of<br>the edge velocity before it saturates. These results are in excellent agreement<br>with theoretical results by Hildings (1997) (both direct numer the edge velocity before it saturates. These results are in excellent agreement with theoretical results by Hildings (1997) (both direct numerical simulation and linear stability calculations), where the base flow was obta with theoretical results by Hildings (1997) (both direct numerical simulation
- (4) The flow visualization shows the formation of three-dimensional well-ordered<br>structures before reattachment. These structures have a spanwise wavelength The flow visualization shows the formation of three-dimensional well-ordered<br>structures before reattachment. These structures have a spanwise wavelength<br>that is about the same as the wavelength of the two-dimensional wave The flow visualization shows the formation of three-dimensional well-or<br>structures before reattachment. These structures have a spanwise waveler<br>that is about the same as the wavelength of the two-dimensional wave. *Phil. Trans. R. Soc. Lond.* A (2000)

*A two-dimensionallaminarseparation bubble* <sup>3205</sup>

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